

## **Influence Of Different Nitrogen And Organic Carbon Sources On Microalgae Growth And Lipid Production**

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**Abstract:** Microalgae based biofuels are getting attention due to energy crisis and environmental protection. In the present study, the *Chlorella* sp. was cultivated in BG-11 medium at batch mode. The effect of different nitrogen (sodium nitrate, potassium nitrate and urea) and organic carbon (glucose, glycerol and sucrose) sources were analyzed on growth and lipid accumulation on this species. The highest biomass growth and biomass productivity of *Chlorella* sp. was found  $1.29 \pm 0.04$  g/l,  $76.96 \pm 4.5$  mg l<sup>-1</sup> d<sup>-1</sup> in urea. However in case of organic sources, the biomass growth and productivity was found maximum in glucose ( $1.43 \pm 0.075$  g/l  $86.04 \pm 3.2$  mg l<sup>-1</sup> d<sup>-1</sup>). The lipid content was examined using Folch method and found better in potassium nitrate nitrogen source (11.84%). Among organic carbon sources, the maximum lipid content (13.22% and lipid yield 189.94 mg/l) were found in case of glucose, followed by glycerol and sucrose. Various properties of biodiesel obtained from *Chlorella* sp. such as Cetane number, Saponification value, Iodine value and Degree of unsaturation were followed standards set by the national petroleum agency (ANP255), ASTM D6751 and EN14214.

**Keywords:** Biodiesel, Biomass growth, *Chlorella* sp., Lipid extraction, Transesterification

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### **I. Introduction**

Energy is backbone of every country's economic development and prosperity. India is the world's fifth largest primary energy consumer and fourth largest petroleum consumer after United States, China and Japan.. India is the world's fifth largest primary energy consumer and fourth largest petroleum consumer after United States, China and Japan. With an outlook for moderate to strong economic growth and a rising population, growing infrastructural and socio-economic development will stimulate an increase in energy consumption across all major sectors of the Indian economy [1]. Transportation is one of the fastest growing sectors using 27% of the primary energy [2]. At the present staggering rates of consumption, the world fossil oil reserves are likely to be exhausted in less than 45 years [3]. Thus, the rising energy (fuel) crisis and environmental degradation have posed a very serious problem to our sustainable growth and survival. So attention has now shifted towards alternative fuels like biodiesel, bio-ethanol and biogas. Biodiesel is fatty acids of ethyl or methyl ester made from virgin or used vegetable oil (either edible or non-edible). The most of the biodiesel production are based on edible oil like soybean oil, rapeseed oil, canola oil or sunflower oil in developed countries. In India the edible oil demand is higher than its domestic production. So there is no possibility of diverting this oil for production of biodiesel. The main commodity sources for biodiesel can be non-edible oils obtained from plant species. There are many species, which bear seeds rich in oil content. Out of these some promising tree species have been identified. These are *Jatropha Curcas* (Ratanjot), *Pongamia Pinnata* (Karanja), *Calophyllum Inophyllum* (Nagchampa or Polanga), Mahua, Castor, Seemarouba etc. Using the current yields, vast amounts of land and fresh water would be needed to produce enough oil to completely replace fossil fuel usage. It would require twice the land area of the US to be devoted to soybean production, or two-thirds to be devoted to rapeseed production, to meet current US heating and transportation needs.

Microalgae are an emerging source for biodiesel production in recent years as due to higher biomass and lipid productivity, and the lack of competition with food crops for agriculture lands and fresh water sources as they can be grow on non-arable land using saline or waste water [4, 5, and 6]. Microalgae are photoautotrophic sunlight-driven cell factories that can convert carbon dioxide to various products such as lipids, carbohydrates, proteins, fatty acids, vitamins, antibiotics, and antioxidants [7]. The lipid content has been increased in many microalgae as a response to severe culture conditions such as CO<sub>2</sub>, nitrogen concentration and light intensity [8]. For the rapid accumulation of lipid, microalgae have been cultured in growth-limiting environment such as nitrogen depletion, [9–11], high light intensity [12], low temperature [13], high salt concentration [14] and high iron concentration [15]. Carbon and nitrogen source changes will greatly affect the biomass and lipid production of microalgae. Dittamart et. al., cultured the *Scenedesmus* sp. AARL G022 under different organic carbon sources such as glucose, glycerol and sodium acetate and found glucose most suitable for biomass growth [16]. Carbon and nitrogen source changes will greatly affect the biomass and lipid production of microalgae. However, to the best of our knowledge, very little attempts have been made on such a

work. Hence, as the pioneering attempts in this direction, the present study focus on microalgae growth and lipid accumulation under different nitrogen and carbon sources

## II. Material And Methods

### 1.1 Microalgae and growth condition

Pure strain of chlorella sp was Yogi Vemana University, Vemanapuram, Kadapa,, Andhra.Pradesh., India and maintained in BBM medium in 250 ml Erlenmeyer flasks containing 100 ml liquid with initial pH 6.8 and incubated under cool florescence light (~2500 lux) at 24°C (±1 °C) with 16 :8 Light. Chlorella sp. was cultured in sterile BG-11 medium at room temperature (~22-36 °C) under cool white, fluorescent lights (with fluorescent illumination of ~3000 lux) for 14 days. One liter bottle was used as a lab scale photobioreator. Working volume of photobioreactor was kept 550 ml with 10% (v/v) inoculum. The photoperiod was set 16:8 light: dark period. The culture was aerated (100 – 200 ml/min) by aquarium pump to avoid settling of algal biomass. Microalgae are cultivated in different nitrogen sources (NaNO<sub>3</sub>, KNO<sub>3</sub>, Urea). But nitrogen content remained same as in BG-11 medium.

Without considering CO<sub>2</sub> in air, the effect of different organic carbon sources (Glucose, Glycerol and Sucrose) were tested with selected optimal Nitrogen Sources. But the carbon content of different organic sources was remained same (0.5gL<sup>-1</sup>).

### Growth analysis and lipid extraction

Microalgae growth was observed by measuring the optical density at 680nm (OD<sub>680</sub>) using UV-visible spectrophotometer (Thermo Scientific) daily and related to algal biomass (g/l). For biomass estimation, 10 ml sample containing algae is filtered through pre-weighted Whatman GF/C glass fiber filter and dry wt. of algae is determined gravimetrically. The relationship developed between OD<sub>680</sub> and biomass (g/l) is given as follows:

$$y=0.3942 \times OD_{680} + 0.0188 \quad (R^2=0.997) \quad (1)$$

Where y is algal biomass in g/l and OD<sub>680</sub> is optical density of culture at 680 nm

The maximum specific growth rate ( $\mu_{max}$  day<sup>-1</sup>) at exponential stage was calculated as follows:

$$\mu_{max} (\text{day}^{-1}) = (\ln X_2 - \ln X_1) / (t_2 - t_1) \quad (2)$$

Where X<sub>1</sub> and X<sub>2</sub> were the dry biomass weight (g/l) at time t<sub>1</sub> and t<sub>2</sub> respectively.

The doubling time (T<sub>D</sub>, days) was calculated as follows:

$$T_D (\text{days}) = \ln(2) / \mu_{max} \quad (3)$$

The rate of biomass production (P, mg L<sup>-1</sup> day<sup>-1</sup>) was calculated by following equation:

$$P (\text{mg L}^{-1} \text{day}^{-1}) = (X_2 - X_1) / t_x \quad (4)$$

Where X<sub>1</sub> and X<sub>2</sub> were the dry biomass weight (g/l) at time t<sub>x</sub>

Lipid was extracted by applying folch extraction method [17].

### 1.2 Fatty acid analysis

The extracted fatty acid is converted in to their methyl esters by transesterification of lipid using 1 ml of 1% NaOH in MeOH followed by heating for 15 minute at 55 °C, adding 2ml of 5% methanolic HCl and again heated for 15 minute at 55 °C, washed by 1ml distilled water. FAME is extracted with hexane (3×1) and evaporated to dryness (18). The fame was re-dissolved in 200µl hexane and analysed using a GC (gas chromatograph) Nucon 5700 series with EOX column (serial no 5061; 30 m length, 0.25 mm ID and 0.25 mm outer dia). Pure Nitrogen (99.9%) used as carrier gas with a flow rate of 1 ml/min and pre-column pressure of 49.7kPa. the initial temperature was set to be 120° C for 2 min, followed by a 4° C/min ramp up to 240° C and maintained for 30 min. the injector and FID detector temperature was set 240° C and 230° C respectively. Fame peaks are identified by comparison of their retention time with authentic standard by GC and quantified by normalization.

### 1.3 Analysis of biodiesel quality

The key qualities of biodiesel the Saponification value (SV), Iodine value (IV), Cetane number (CN) and (DU) degree of unsaturation values were calculated by using empirical Eq. 5-8 (19 20).

$$SV = \Sigma (560 \times N) / MW \tag{5}$$

$$IV = \Sigma (254 \times N \times D) / MW \tag{6}$$

$$CN = (46.3 + 5458 / SV) - (0.225 \times IV) \tag{7}$$

$$DU = (MUFA, wt \%) + (2 \times PUFA, wt \%) \tag{8}$$

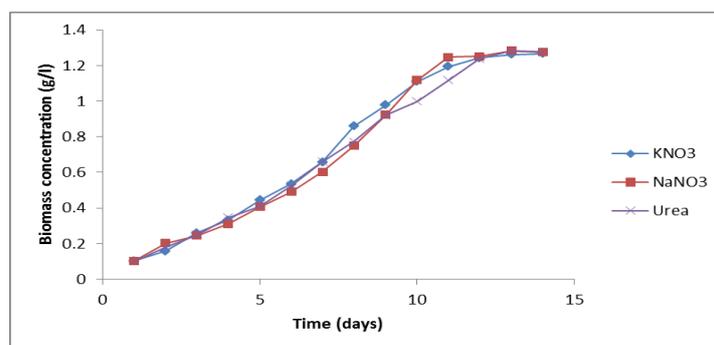
Where N is the percentage of each fatty acid, MW is the molecular mass of fatty acid, D is the number of double bonds, MUFA is monounsaturated fatty acids and PUFA is polyunsaturated fatty acid by wt. %.

During the entire experiment, the measurements of the values were done in triplicates and the mean and  $\pm$  standard deviation (SD) was calculated using GraphPad Prism 6 statistical software.

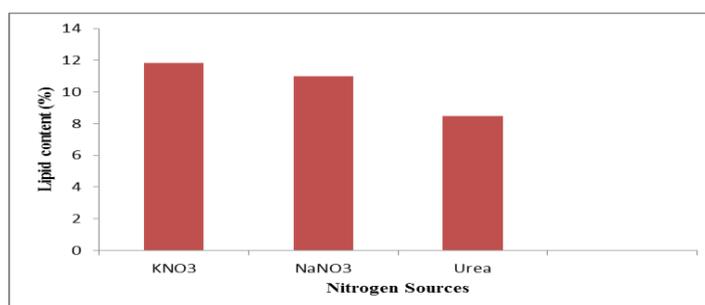
### III. Results & Discussion

#### 1.4 Biomass and Lipid accumulation of chlorella sp. at different nitrogen sources

In this study, Chlorella sp. was grown in Bg-11 for 14 days and source of nitrogen sodium nitrate is replaced by KNO<sub>3</sub>, and Urea. The effect of different nitrogen sources on Chlorella sp. is shown in fig 1. It was observed that Chlorella sp. shows higher biomass content (1.29 $\pm$ 0.04 g/l) in Urea, followed by sodium nitrate (1.28  $\pm$ 0.11 g/l and KNO<sub>3</sub> (1.26 $\pm$ 0.05 g/l ). The specific growth, doubling time, biomass productivity and lipid yield at stationary phase are shown in table 1. Highest specific growth and biomass productivity was observed 0.19369 $\pm$ 0.0058 day<sup>-1</sup> and 76.96 $\pm$ 4.5 mg/l/day in urea while lowest was 0.192457 $\pm$ 0.0044 day<sup>-1</sup> and 74.92 $\pm$ 3.3 mg/l/day in KNO<sub>3</sub>. The doubling time of microalgae biomass was minimum in urea (3.58 $\pm$ .105 days), followed by KNO<sub>3</sub> (3.60 $\pm$ .088 days) and NaNO<sub>3</sub> (3.62 $\pm$ .169 days). Maximum lipid content was recorded 11.83 $\pm$ 1.8% for KNO<sub>3</sub> while minimum lipid content was found in case of urea (8.49%). However, the lipid yield was found better for KNO<sub>3</sub> (149.65 $\pm$ 4.8 mg/ml), followed by NaNO<sub>3</sub> (141.21 $\pm$ 10.63 mg/ml) and urea (109.01 $\pm$ 10.85 mg/ml). [Qiang Lin](#) examined the effects of nitrogen source ((NH<sub>4</sub>)<sub>2</sub>CO<sub>3</sub>, urea, NaNO<sub>3</sub>, urea and NaNO<sub>3</sub> mixture) and concentration on the ash free dry biomass (AFDB) and oil accumulation and productivity of a Scenedesmus rubescens and found that the microalgae nurtured with the mixture of urea-N and NaNO<sub>3</sub>-N had the highest AFDB productivity of 0.539  $\pm$  0.040 g/L/d and the content of fatty acid methyl esters (FAME) (%) fed with (NH<sub>4</sub>)<sub>2</sub>CO<sub>3</sub>-N increased continuously for 17 days and reached 42.94  $\pm$  2.05% in the indoor photo-bioreactors (21). Muthu Arumugam also investigated the influence of different nitrogen source (potassium nitrate, sodium nitrate, urea, calcium nitrate, ammonium nitrate and ammonium chloride) of varying concentrations on biomass production of green algae Scenedesmus and found nitrate was the promising source for growth of Scenedesmus at low concentration (22).



**Fig.1. Dry weight of Chlorella sp. under different nitrogen sources**



**Fig.2. Lipid content of Chlorella sp. under different nitrogen sources**

**Table 1. Growth characterization of Chlorella sp. under different nitrogen sources**

| Nitrogen sources  | Specific growth ( $\mu_{max}$ ) Day <sup>-1</sup> | Doubling time | Rate of biomass (mg l <sup>-1</sup> day <sup>-1</sup> ) | Lipid yield at the end of experiment (mg/l) |
|-------------------|---|---------------|---|---|
| NaNO <sub>3</sub> | 0.192±0.0066                                      | 3.62±0.169    | 75.98±7.7   | 141.21±10.63                                |
| KNO <sub>3</sub>  | 0.192457±0.0044                                   | 3.60±0.082    | 74.92±3.3   | 149.654.8                                   |
| Urea              | 0.19369±0.0058                                    | 3.58±.105     | 76.96±4.5   | 109.01±10.85                                |

### 3.2 Biomass and Lipid accumulation of chlorella sp. and chlorella pyronidisa at different Carbon sources

After achieving optimal nitrogen sources, Chlorella species were grown in different organic carbon sources such as Glucose, Glycerol and Sucrose (shown in Fig.3). At stationary phase, it was observed that addition of glucose resulted in maximum biomass productivity of 86.04±3.2 mg l<sup>-1</sup>day<sup>-1</sup> while addition of sucrose and glycerol results in 69.38±9.2 and 80.39±3.9 mg l<sup>-1</sup>day<sup>-1</sup> respectively. The specific growth and doubling time was found better in glucose (0.197±0.002 day<sup>-1</sup> and 3.50±0.04 day), followed by glycerol (0.196±0.0026 day<sup>-1</sup> and 3.53±0.04 day) and sucrose (0.186±0.0016 day<sup>-1</sup> and 3.73±0.21day). The lipid content and lipid yield of Chlorella sp. also found maximum 13.22± 0.86%, 189.94 ±8.95 mg/l in glucose in comparison to glycerol (11.28667±1.15% and 163.72±7.6 mg/l) and sucrose (12.18 ± 0.87 and 109.04±10.8 mg/l). In the study of Dittamart et. al. (2014) the most suitable carbon source was found to be 0.05M glucose, giving a yield of 2.78 ± 0.86 g./l of biomass and 233.68 ± 35.34 mg.L-1 of crude lipid (16). Gim et. al. (2013) also cultivated chlorella vulgaris in different organic carbon sources and observed glucose as better source for growth enhancement (23). This is mainly due to that the glucose is a simple hexose monosaccharide, which is first catabolized glucose-6-phosphate (important intermediate product for various metabolic precursors) and subsequently to pyruvate through anaerobic glycolysis process, and then entered into TCA cycle followed by mitochondrial oxidative phosphorylation for ATPs production (23, 24, 25).

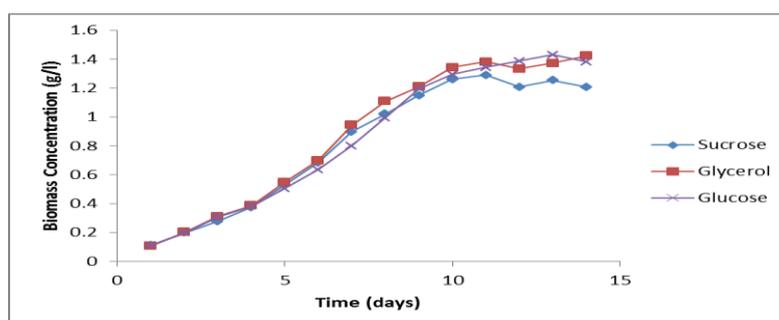


Fig.3. Dry weight of Chlorella sp. under different organic carbon sources

### 3.3 Fatty acid composition and Fuel properties of chlorella sp.

Fig 5 shows fatty acid composition of chlorella sp. and it was observed that Chlorella sp. contain 45.21% saturated FAME, 22.56% mono saturated FAME and 22.56% poly saturated FAME. According to European standards EN14214, for an ideal biodiesel the percentage of linolenic acid (C18:3) and polyunsaturated FA (>4 double bond) should not increase 12% and 1% respectively. In the present study C18:3 for Chlorella sp. are 4.54% and C18:4 is absent which makes it stable for fuel application.. Different Physico chemical properties of fuel obtained from this species were shown in table 3.

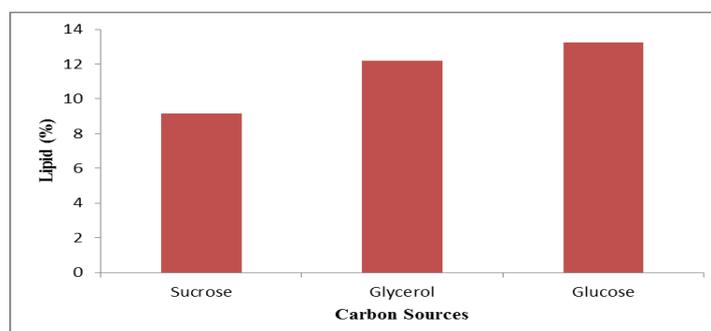


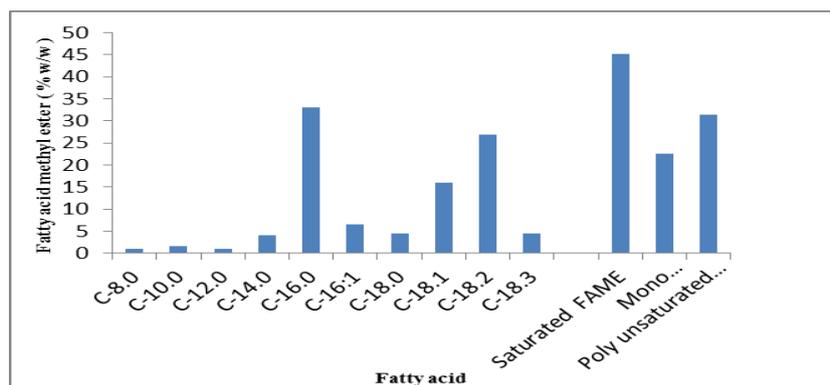
Fig.4. Lipid content of Chlorella sp. under different carbon sources

**Table 2 Growth characterization of *Chlorella* sp. under different Carbon sources**

| Carbon sources | Specific growth ( $\mu_{max}$ ) Day <sup>-1</sup> | Doubling time | Rate of biomass mg l <sup>-1</sup> day <sup>-1</sup> | Lipid yield at the end of experiment (mg/l) |
|----------------|---|---------------|--|---|
| Sucrose        | 0.186±0.0016                                      | 3.73±0.21     | 69.38±9.2  | 109.04±10.8                                 |
| Glycerol       | 0.196±0.0026                                      | 3.53±0.04     | 80.39±3.9  | 163.72±7.6                                  |
| Glucose        | 0.197±0.002                                       | 3.50±0.04     | 86.04±3.2  | 189.94±8.15                                 |

**Table 3 Physico-chemical characterization of *Chlorella* sp**

| Properties           | SV    | IV    | CN   | DU    | References |
|----------------------|-------|-------|------|-------|------------|
| <i>Chlorella</i> sp. | 00.43 | 26.59 | 5.04 | 45.26 | This study |
| <i>Chlorella</i> sp. | 217.8 | 65    | 56.7 | 74.1  | (28)       |
| Sunflower            | -     | -     | 50   | 152.2 | (29)       |



**Fig.5 Fatty acid composition of *Chlorella* sp.**

#### IV. Conclusion

In the present study, the growth and total lipid contents of *Chlorella* sp. was compared in different nitrogen and organic carbon sources. Comparing to sodium nitrate, higher lipid yield was observed in potassium nitrate. The addition of organic carbon sources in control medium results in higher biomass growth and lipid medium. Among the various carbon sources tested, glucose was the best organic carbon source for *Chlorella* sp. and lipid yield was found maximum (189.94±8.15) in comparison to other organic carbon sources. The presence of more than 60 % saturated and mono saturated fatty acid in *Chlorella* sp. prove that it is a good candidate for biodiesel production. The quality and properties of biodiesel met the criteria of the national petroleum agency (ANP255), Standard ASTM D6751 and European standards (EN 14214).

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