

MHD MIXED CONVECTION FLOW OF WATER AT 4°C PAST A VERTICAL POROUS PLATE UNDER CHEMICAL REACTION AND SUCTION

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Abstract: Flow of water at its maximum density past a porous vertical plate is considered. Effects of a transversely applied magnetic field, first order chemical reaction and suction of the plate on the flow field are studied by a similarity transformation of the governing equations. For various values of the magnetic, chemical reaction and suction parameters numerical values proportionate to Skin friction, Nusselt number and Sherwood number are tabulated and graphical results for the velocity, temperature and concentration profiles are presented. Computed values and graphical results for flow of water at a normal temperature are compared with that of flow at 4°C.

Key words: Maximum density of water, porous plate, Chemical reaction, suction, Prandtl number

I. Introduction

Flow of electrically conducting fluid past a vertical plate is a widely studied problem in fluid dynamics. The fact that magnetic field has profound influence on boundary layer flow of an electrically conducting fluid, has attracted the attention of researchers due to its various applications in plasma physics, nuclear science, engineering design and space dynamics. Such flows are termed as MHD flows in the broader sense and abundant literature reviews are available concerning MHD convective flow of fluid past a vertical plate.

Convection heat transfer coefficients, natural or forced, are a strong function of the fluid velocity. In dealing with forced convection flow we generally ignore the effects of free convection. Similarly we assume the forced convection as negligible while dealing with free convection flow. The error involved in ignoring natural convection while studying forced convection is negligible at high velocities but may be considerable at low velocities. Situations may arise for which free and forced convection effects are comparable, in which case it is inappropriate to neglect either process. Therefore it is desirable to have a criterion to assess the relative magnitude of natural convection in the presence of forced convection flows. Such flows situations where both free and forced convection effects are of comparable order belong to the mixed convection regime. In several practical applications of heat transfer theory to the vertical plate problems there exists significant temperature difference between the surface of the hot plate and the free stream. This temperature difference cause density gradients in the fluid medium and in the presence of a gravitational body force, free convection effects become important. It has generally been recognized that $\lambda = \frac{Gr}{Re^2}$, where Gr is the Grashof number and Re the Reynolds

number is the governing parameter for the laminar boundary layer forced-free mixed convection flow which represents the ratio of the buoyancy forces to the inertial forces inside the boundary layer. Forced convection exists when $\lambda \rightarrow 0$ which occurs at the leading edge and the free convection limit can be reached if λ becomes large. We know from authoritative work in heat transfer [1] that free convection is negligible if $\lambda \leq 1$ and forced convection is negligible if $\lambda \geq 1$. Hence combined free and forced (or mixed) convection regime is generally one for which $\lambda \approx 1$. Although the flows with only one of the two effects involved will have a self similar character, such situations will mathematically lead to ordinary differential equations and are easy to solve. But as soon as the two effects occur together, boundary value problem involving partial differential equations will arise and are not easy to solve by conventional procedures. The physical explanation of the complexities is that the two effects act differently with respect to the characteristic length l and any combination means that the characteristic length is introduced into the problem (i.e., the length from the leading edge to the separation position). If both the effects are to be considered, pure forced convection always dominates for $l \rightarrow 0$ while direct natural convection dominates for $l \rightarrow \infty$. Most of the works concerning external flows past a vertical plate are either considered for free or forced convection regimes only. However mixed convection flows received considerable attention in the late 1970s to 1980s and numerous literature reviews are available [2]-[4].

In nature it is rather impossible to find pure fluid unless special efforts are made to obtain it. The most common fluids like water, air etc. are contaminated with impurities like CO_2 , C_6H_6 , H_2SO_4 etc. and generally we have to consider presence of such foreign mass while studying flows past different bodies. In such a case the density

difference in the fluid is caused by material constitution in addition to temperature differences. The common example of such a flow is the atmospheric flow which is driven appreciably by both temperature and H₂O concentration differences. When such contaminant is present in the fluid under consideration there does occur some chemical reaction e.g. air and benzene react chemically, so also water and sulfuric acid. During such chemical reactions, there is always generation of heat. But when the foreign mass present in the fluid at very low level, we can assume a first order chemical reaction and the heat generated due to chemical reaction can be very negligible. Several authors have done significant works by taking into account a first order chemical reaction on flow past vertical surfaces [5]-[7].

Water is an intriguing substance that plays a vital role in sustaining life on earth. Despite being the most abundant liquid on earth, it is also the most anomalous. Some of these anomalous properties make water particularly well adapted for its various roles in sustaining life on the planet. When liquid water freezes, it becomes less dense. Contrary to the behavior of most other solids, water expands on freezing and the solid state is less dense than the liquid state. This behavior has a significant impact on aquatic life for keeping ice at the top of ponds and lakes during cold winters allowing aquatic life to survive at the bottom where warm water circulates. Another property of water that is exploited by aquatic life to survive under such cold conditions is the colligative nature of its freezing point. When a solute such as sodium chloride or sucrose is added to water the temperature at which it freezes is lowered. The physical properties of water such as the thermal conductivity, the specific heat capacity, the viscosity and the density are linear functions of temperature [1]. A notable exception to this linear variation is liquid water which at a pressure of one atmosphere has a maximum density of 999.9720 kg/m³ at 4⁰C. Above this temperature, the density of water decreases as the temperature is increased in a manner similar to other fluids. For temperature below 4⁰C the trend is reversed, density increases with increased temperature giving rise to the maximum density at 4⁰C. This type of parabolic variation of the density of water as a function of temperature was reported for the first time by Goren [8]. After that phenomenal interest grew around this anomaly among various researchers in doing experimental as well as theoretical [9]-[18] studies. However, effects of chemical reaction and suction on the flow of water at maximum density have not been considered in the literature so far, which remained as a motivating cause to undertake this study.

The driving mechanism of the convective flows is described by the buoyancy term in the momentum equation of the governing equations. As a consequence of this, the order of magnitude of all terms in this equation is dictated by the buoyancy term. However, this buoyancy term came up as a consequence of expanding the density in a Taylor series and taking only the linear term into account and ignoring all other terms as follows:

$$\begin{aligned} \rho(T) &= \rho_{\infty} + \left(\frac{\partial \rho}{\partial T}\right)_{\infty} (T - T_{\infty}) + \left(\frac{\partial^2 \rho}{\partial T^2}\right)_{\infty} \frac{(T - T_{\infty})^2}{2!} + \left(\frac{\partial^3 \rho}{\partial T^3}\right)_{\infty} \frac{(T - T_{\infty})^3}{3!} + \dots \\ &= \rho_{\infty} \left[1 - \left\{ -\frac{1}{\rho_{\infty}} \left(\frac{\partial \rho}{\partial T}\right)_{\infty} \right\} (T - T_{\infty}) - \left\{ -\frac{1}{\rho_{\infty}} \left(\frac{\partial^2 \rho}{\partial T^2}\right)_{\infty} \right\} \frac{(T - T_{\infty})^2}{2!} - \dots \right] \\ &= \rho_{\infty} \left[1 - \beta_{\infty} (T - T_{\infty}) - \left\{ -\frac{1}{\rho_{\infty}} \left(\frac{\partial^2 \rho}{\partial T^2}\right)_{\infty} \right\} \frac{(T - T_{\infty})^2}{2!} - \dots \right] \\ \frac{\rho(T) - \rho_{\infty}}{\rho_{\infty}} &= -\beta_{\infty} (T - T_{\infty}) - \beta^*_{\infty} (T - T_{\infty})^2 - \dots \end{aligned}$$

Here $\beta_{\infty} = -\frac{1}{\rho_{\infty}} \left(\frac{\partial \rho}{\partial T}\right)_{\infty}$ is the coefficient of thermal expansion at temperature T_{∞} . While invoking the Boussinesq approximation, it is generally assumed that β_{∞} does not vanish, but for water at 4⁰C the density is maximum and consequently β_{∞} becomes equal to zero. Considering this fact into account, Goren [8] has shown that for temperature sufficiently close to $T_c = 3.98^{\circ}\text{C}$, the relationship between fluid temperature T and the density ρ_c is given by the relation:

$$\frac{\rho(T) - \rho_c}{\rho_c} = -\beta^*_{\infty} (T - T_c)^2 \tag{1}$$

Where ρ_c the maximum density in the liquid is phase and $\beta^*_{\infty} = 8.0 \times 10^{-6} (\text{C})^{-2}$ is the thermal expansion coefficient of water at 4⁰C. This type of parabolic variation in density has attracted the attention of many researchers and several authors have done significant work taking up the flow of water at its maximum density [9]-[18].

II. Formulation Of The Problem:

A two-dimensional combined free-forced convective flow of water at its maximum density along a semi-infinite vertical isothermal porous plate under suction is considered. The flow is assumed to be in the direction of x axis which is taken along the vertical plate in the upward direction and the y axis is taken to be normal to the plate. Let u and v be the components of velocities of the fluid along x and y axis respectively. Flow configuration is

shown in Fig.1. A transverse magnetic field of uniform strength B_0 is applied normal to the flow and the induced magnetic field is neglected. Initially the surface of the plate is at the same free stream temperature T_∞ and the uniform free stream velocity u_∞ parallel to the vertical plate. The plate temperature is raised to T_w ($T_w > T > T_\infty$). We neglect Dufour and Soret effects and viscous dissipation and assume all fluid properties as constant except variation of density. Then making use of (1), under the usual Boussinesq approximation the boundary layer equations based on the conservation of mass, momentum and energy, governing the flow problem can be expressed as:

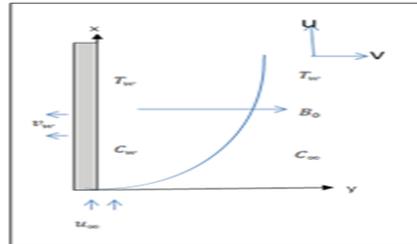


Figure 1

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (2)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = g\beta(T - T_\infty) + g\beta^*(C - C_\infty) - \frac{\sigma B_0^2}{\rho}(u - u_\infty) \quad (3)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha \frac{\partial^2 T}{\partial y^2} \quad (4)$$

$$u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} = D \frac{\partial^2 C}{\partial y^2} - k_1(C - C_\infty) \quad (5)$$

The initial and boundary conditions are :

$$\text{For } y = 0 : u = 0, v = -v_w, T = T_w, C = C_w$$

$$\text{For } y \rightarrow \infty : u = u_\infty, T \rightarrow T_\infty, C \rightarrow C_\infty \quad (6)$$

Here the x axis is taken along the plate in the vertically upward direction and the y axis is taken normal to the plate. u and v are the velocity components along x and y respectively. T is the fluid temperature, C is the species concentration, T_∞ is the ambient temperature, C_∞ is the ambient concentration, g is the acceleration due to gravity, ρ is the fluid density, β is the volumetric coefficient of thermal expansion, β^* is the volumetric coefficient of expansion with concentration, σ is the electrical conductivity, B_0 is the magnetic field flux density, D is mass diffusion coefficient, α is the thermal diffusivity and k_1 the chemical reaction coefficient. The suction velocity of the plate is $v_w (> 0)$. Now we introduce the following similarity variables:

$$\eta = y \sqrt{\frac{u_\infty}{\nu x}}, \quad \psi(x, y) = \sqrt{u_\infty \nu x} f(\eta) \quad (7)$$

Where the velocity components are given by

$$u = \frac{\partial \psi}{\partial y}, \quad v = -\frac{\partial \psi}{\partial x} \quad (8)$$

With the help of (7) and (8), the governing equations (2)-(5) and the boundary conditions (6) take the form:

$$f''' + \frac{1}{2} f f'' + \lambda_1 \theta^2 + \lambda_2 \varphi - M(f' - 1) = 0 \quad (9)$$

$$\theta'' + \frac{1}{2} Pr f \theta' - Pr f' \theta = 0 \quad (10)$$

$$\varphi'' + \frac{1}{2} Sc f \varphi' - \gamma Sc Re \varphi = 0 \quad (11)$$

The transformed boundary conditions are:

$$f' = 0, f = f_w, \theta = 1, \varphi = 1 \text{ at } \eta = 0,$$

$$f' \rightarrow 1, \theta \rightarrow 0, \varphi \rightarrow 0 \text{ as } \eta \rightarrow \infty \quad (12)$$

Here $\theta = \frac{T - T_\infty}{T_w - T_\infty}$, $\varphi = \frac{C - C_\infty}{C_w - C_\infty}$, $G = \frac{g\beta(T_w - T_\infty)x^3}{\nu^2}$ is the thermal Grashof number, $Re = \frac{u_\infty x}{\nu}$ is the Reynolds number

for water at 4⁰C, $G^* = \frac{g\beta_C(C_w - C_\infty)x^3}{\nu^2}$ is the mass Grashof number, $\lambda_1 = \frac{G}{Re^2}$ and $\lambda_2 = \frac{G^*}{Re^2}$ are respectively the

thermal and mass buoyancy parameters of mixed convection, $M = \frac{\sigma B_0^2 x}{\rho u_\infty}$ is the magnetic parameter, $Pr = \frac{\nu}{\alpha} = 11.4$ is the Prandtl number for water at 4⁰C, $Pr = 7.0$ for water at 20⁰C, $\gamma = \frac{k_1 \nu}{u_\infty^2}$ the chemical reaction parameter and $Sc = \frac{\nu}{D}$ is the Schmidt number of a soluble species in water. $f_w = 2 \sqrt{\frac{x}{\nu u_\infty}} v_w$ is the suction parameter and dashes denote differentiation with respect to the similarity variable η . Knowing the velocity field, the physical quantities of interest to our study are the Skin friction $C_f = \frac{2\tau_w}{\rho u_\infty^2}$ which is given by the wall shear stress $\tau_w = \left[\mu \left(\frac{\partial u}{\partial y} \right) \right]_{y=0}$, the Local Nusselt number $Nu = \frac{x q_w}{k(T_w - T_\infty)}$ given by the heat flux $q_w = -k \left(\frac{\partial T}{\partial y} \right)_{y=0}$ and the Local Sherwood number $Sh = \frac{x M_w}{D(C_w - C_\infty)}$ given by the mass flux $M_w = -D \left[\frac{\partial C}{\partial y} \right]_{y=0}$.

In view of (12), the Skin Friction coefficient C_f reduces to

$$\frac{1}{2} C_f (Re)^{\frac{1}{2}} = f''(0) \tag{13}$$

the Nusselt number Nu reduces to

$$Nu(Re)^{-\frac{1}{2}} = -\theta'(0) \tag{14}$$

the Sherwood number Sh reduces to

$$Sh(Re)^{-\frac{1}{2}} = -\varphi'(0) \tag{15}$$

III. SOLUTION OF THE PROBLEM:

The non-linear coupled system of equations (9) – (11) along with the boundary conditions (12) are solved numerically using the continuation method with the help of the inbuilt Matlab routine for solving two point boundary value problems numerically for a fixed value of the buoyancy parameters $\lambda_1 = \lambda_2 = 0.5$, different values of the magnetic parameter M and the chemical reaction parameter γ and suction parameter f_w . During computation, the Prandtl number $Pr = 11.4$, the Schmidt number $Sc = 500$ for an arbitrary species and Reynolds number $Re = 10^3$ chosen arbitrarily for water at 4⁰C. We want to investigate the chemical reaction, suction and magnetic effects on the flow field and as such keeping all other parameters fixed will highlight the effects clearly. Graphical results for 4⁰C are compared to the case of flow of water at 20⁰C. The numerical values for both the two flow fields in $f''(0), \{-\theta'(0)\}$ and $\{-\varphi'(0)\}$ are evaluated and are listed in Table 1.

Table 1										
$\frac{G}{Re^2} = 0.5 = \frac{G^*}{Re^2}, Sc = 500, Re = 10^3$										
M	γ	f_w	Water at 4 ⁰ C			Water at 20 ⁰ C			Profile	Fig.no
			$f''(0)$	$-\theta'(0)$	$-\varphi'(0)$	$f''(0)$	$-\theta'(0)$	$-\varphi'(0)$		
0	1	1	0.7701	5.9854		0.8455	3.8857			
1	1	1	1.3763	6.1332	843.0704	1.4351	4.0357	843.0704	Velocity	2
2	1	1	1.7606	6.2105		1.8126	4.1116		Temperature	3
3	1	1	2.0651	6.2650		2.1129	4.1641			
1	0	1	1.3777	6.1333		1.4365	4.0358			
1	1	1	1.3763	6.1333	843.0704	1.4351	4.0357	843.0704	Velocity	4
1	2	1	1.3762	6.1332		1.4349	4.0357		Temperature	5
1	3	1	1.3761	6.1332		1.4349	4.0357			
1	1	0	1.1378	1.7347		1.2086	1.4883			
1	1	1	1.3763	6.1333	843.0704	1.4351	4.0357	843.0704	Velocity	6
1	1	2	1.7049	11.5807		1.7456	7.2564		Temperature	7
1	1	3	2.0823	17.2052		2.1121	10.6562			

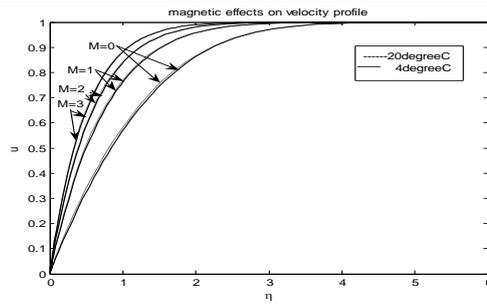


Figure2

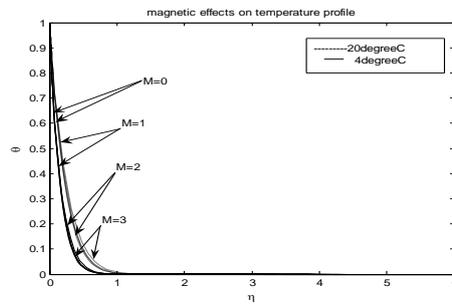


Figure3

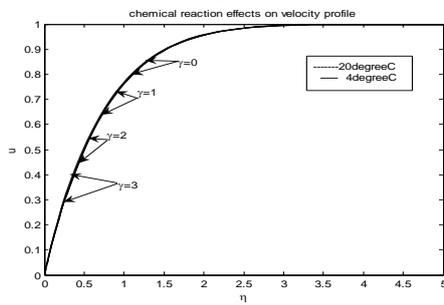


Figure4

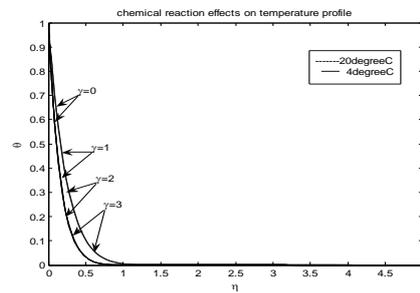


Figure5

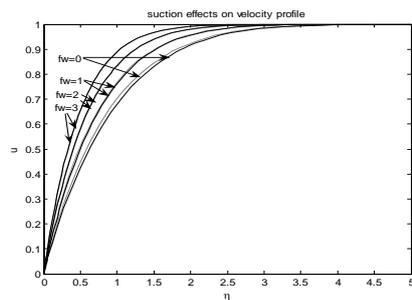


Figure6

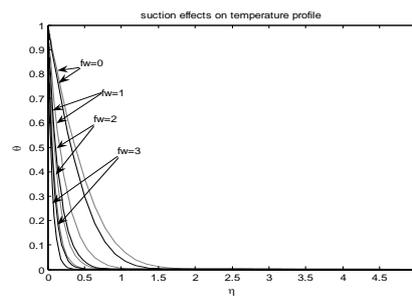


Figure7

IV. Conclusions:

- (i) Magnetic effect on both the two flow fields is almost identical with a slight reduction in the velocity in the case of 4⁰C but the effect on the temperature profile is significant with a reducing effect for 4⁰C.
- (ii) Chemical reaction has no significant effect on the velocity profile but has a reducing effect on the temperature profile.
- (iii) Suction has a slight retarding effect on the velocity profile but has a considerable retarding effect on the temperature field for 4⁰C.
- (iv) Concentration profile remained unaffected in all the cases in both the flow fields.

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